

Original Research Article

Batch adsorption removal of Nickel and Cadmium metal ion from wastewater using Waste material of Fabrics as Adsorbent

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ABSTRACT

The current research presents texture fly ash as an adsorbent for adsorption of Nickel and Cadmium metal ions from the aqueous solution. All tests to examine the impact of parameters, for example, pH and adsorbent measurements were done at 35 °C. The outcomes settled based on their ideal range for pH 6.8 and 0.1 g of adsorbent measurement. Mechanism of adsorption was clarified by Temkin isotherm that portrays the association of adsorbate and adsorbent. Adsorption binding isotherm constant and heat of adsorption expanded as temperatures expanded to 35 °C, 45 °C and 55 °C for Nickel metal ion, on another part for Cadmium metal ion binding constant consistent esteem expanded, however, the heat of adsorption diminished. A kinetic report was improved for the three temperatures 35 °C, 45°C and 55 °C. Kinetic behavior clarified by Pseudo-second request, Weber-Morris model, and Elovich second order equation.

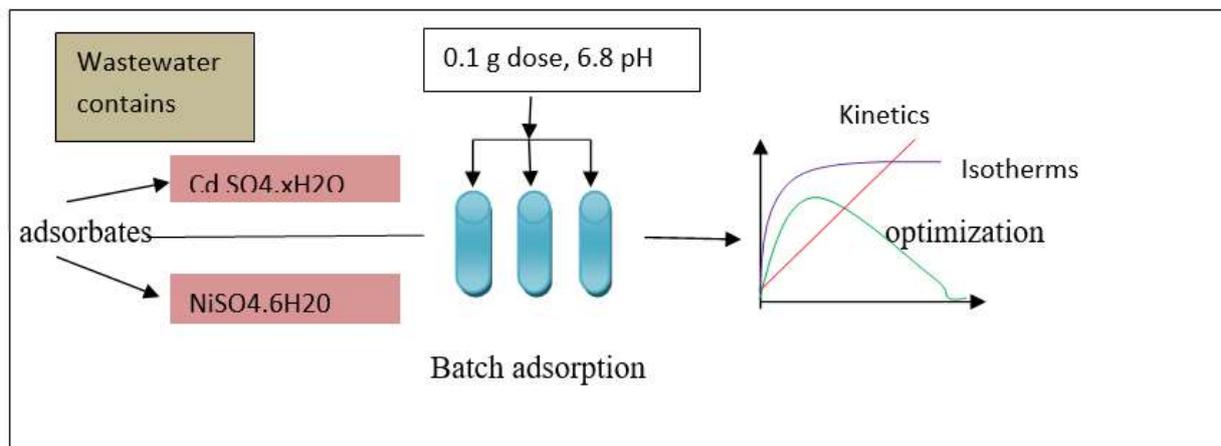
KEYWORDS

Adsorption | Cadmium | Nickel | Fabric Fly Ash | Isotherm | Kinetic

CITATION

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Introduction



Present century polluted water is of major concern for all living organisms (Rezvani *et al.*, 2018). Polluted water released by various industrial sectors as well as domestic waste. But water released by industrial sectors contains many precious metals, so it has become necessary to remove these metals. These metals are heavy metals, precious metals as well as nutrient metals. If these heavy metals are taken by human beings in lesser quantity, then they play the role of nutrient metal for human body growth, but when these heavy metals limit exceed by permissible limit, then they play the role of toxic metals not only for the human body also for living organism. They may cause many serious diseases like cancer, kidney failure, high and low blood pressure, headache, nausea, vomiting, etc (Tchounwou *et al.*, 2012). So to stop this degradation of the environment, it is necessary to remove these heavy metals.

Heavy metals are metals which have high atomic weight, high density, and high specific gravity. There is some heavy metals available in periodic table, but some important and toxic heavy metals are cadmium, mercury, lead, arsenic, manganese, chromium, cobalt,

nickel, copper, zinc, selenium, silver, antimony, and thallium. Some of the heavy metals are released by various industries like electroplating, mining, automobile, pharmacy, textile and dyes, chromate manufacturing, leather tanning, aluminum production, metal cleaning, and processing sectors (Ertugay *et al.*, 2008; Jain *et al.*, 2009; Prabu *et al.*, 2012). So the far number of methods available such as ion exchange, electro dialysis, membrane filtration, reverse osmosis, chemical precipitation and adsorption (Fu and Wang 2011). Conventional treatment methods offer high capital cost and undesirable percentage removal whereas biosorption has found on past researcher analysis very potent and efficacious method as it offers affordable and trouble free quality and provides high percentage removal (Kadirvelu *et al.*, 2001; Ricordel *et al.*, 2001; Tiwari *et al.*, 2015).

Nickel is a non-biodegradable toxic metal ion, and the presence of Ni (II) ions in drinking water may cause adverse health effects such as anemia, diarrhea, encephalopathy, hepatitis, lung and kidney damage, gastrointestinal distress, pulmonary fibrosis, renal edema, skin dermatitis, and central

nervous system dysfunction (Zhang *et al.*, 2015; Khan *et al.*, 2012).

Cadmium is widely used and extremely toxic in relatively low dosages, is one of the principal heavy metals responsible for causing kidney damage, renal disorder, high blood pressure, bone fracture and destruction of red blood Cells (Kumar *et al.*, 2010).

As bunches of adsorbents, for example, activated carbon (Eleni *et al.*, 2015; Manjuladevi *et al.*, 2018), zeolites (kocaoba *et al.*, 2007; Taamneh *et al.*, 2017; Zendelska *et al.*, 2015), biomass (Mahmood *et al.*, 2017; Vakili *et al.*, 2014), fly ash (Sridevi *et al.*, 2013), plant materials (Emenike *et al.*, 2016; Samuel *et al.*, 2016), and so forth have prevailed in expulsion and provide high adsorption limit (Barakat, 2011; Keng *et al.*, 2014). The point of the Present examination to present texture of fly ash remains as an adsorbent for adsorption of Nickel and Cadmium metal ions. Waste cloth fabric ash provides better removal efficiency, so it has demonstrated as minimal effort and productive adsorbent. The adsorption of metal ions has never been reported by waste cloth fabric ash. Nettle ash has reported by one researcher (Mousavi and Seyedi 2011) and revealed adsorption efficiency 192.3 and 142.8 mg/g for cadmium and nickel metal ion. Novelty of the work is to exploit waste cloth fabric ash as adsorbent.

Materials and methods

Adsorbent utilised

As some little bits of textures are dealt with as waste which is, for the most part, tossed at junk level. Along these lines, to limit the misuse of the material business, Waste fabric tests were gathered from around territories.

Material texture at that point washed and dried in daylight till totally dry and after then totally consume within the sight of oxygen at the open territory. The physio-substance properties of the sample gives better description as detailed by (Page *et al.*, 1979). Moisture content of substance, pH, and specific gravity were found as 70%, 6.8 and 1.5 g ml^{-1} . Surface area found to be $50.876 \text{ m}^2/\text{g}$.

Adsorbate used

The synthetic compounds were utilized as Cadmium sulfate hydrate and Nickel (II) sulfate hexahydrate salts in batch adsorption study. For tests, these salts were utilized to get ready 25 ppm stock solution by dissolving in refined water. Impacts of parameters initial metal ion concentration, pH, and adsorbent measurements were contemplated independently. pH of the arrangement is balanced by 0.1 N HCl and 0.1 N H_2SO_4 . Every one of the tests was directed by differing one of a factor while other staying settled at $35 \text{ }^\circ\text{C}$. The wavelength (390 and 373nm) selected for both Cadmium and Nickel metal ions.

Instruments used

Absorbance was checked by UV-Vis spectrophotometer RIGOL Ultra 3660 for all adsorption studies available in the university. Perkin Elmer Frontier instrument was utilized to characterize for morphological image and XRD image which was available in Punjab University Chandigarh. Nitrogen adsorption-desorption isotherm and surface area were examined with the help of Quanta Chrome Nova 1000.

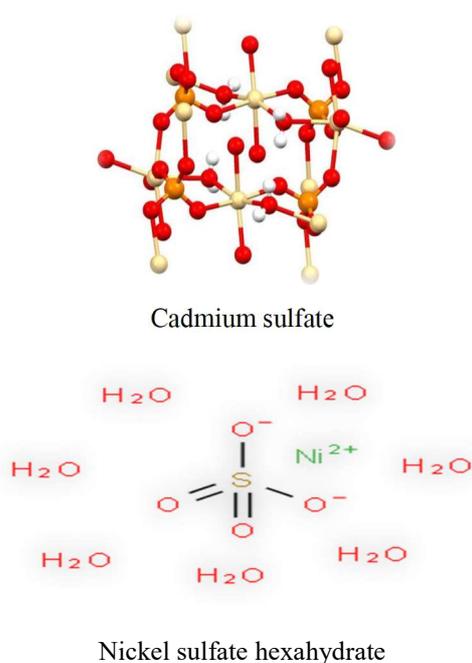


Fig. 1 structure of adsorbate molecules

Results and Discussion

Characterization of adsorbent

This testing of the adsorbent sample indicates the presence of the functional group. A presence of functional groups decides the adsorption behavior of adsorbent or tells about the mechanism of the adsorption reaction. An indication of a hydroxyl group, alcoholic group, -NH stretching and ethers shows the effective adsorption. Perkin Elmer Frontier model was used to characterize.

Comparison of FTIR band positions at different functional groups before adsorption and after adsorption obtained in the range 400 cm^{-1} to 4000 cm^{-1} with numerous groups as shown in Table 1. Broad peak was obtained at 3440 cm^{-1} and 1626 cm^{-1} , N-H stretching 1462 cm^{-1} , C-O vibrations 1014 cm^{-1} . After adsorption peaks were shifted to other intensity due to the interaction of surface-ion. A similar trend reported somewhere (He *et al.*, 2016; Muinde *et al.*, 2017)

WCFA adsorbent	Before adsorption	After adsorption
Coupled with H-bond	3440	3418
Ring stretches of C=C	1626	1648
Ring stretches N-H	1462	1430
Aromatic C-H deformation	1014	1014

Table 1: FTIR information for the fabric fly ash before and after adsorption

Scanning Electron Morphology (SEM): this morphology test introduces the morphological image of the sample when a beam of electrons spread over the sample. It tells about the porous structure of the sample and the presence of cavities which is in favorable to adsorption (Visa *et al.*, 2014). Images of sample adsorbent shows rough surface at $10\text{ }\mu\text{m}$ and $20\text{ }\mu\text{m}$. both average sizes image evident that adsorbent sample have sufficient pore size for adsorbates to adsorb.

BET nitrogen adsorption-desorption isotherm: the plot of adsorption-desorption nitrogen isotherm between relative pressure vs. volume adsorbed presents the amount of nitrogen gas adsorbed on to the surface of adsorbent as well as amount of that gas desorbs at constant temperature of 77K . This amount of gas adsorbs into the mesopore area due to high temperature operation and this mesoporosity is revealed by hysteresis behavior as shown in figure 4. A same trend presented by (Boycheva *et al.*, 2016).

XRD: XRD technique is very identical that determines the strength of unknown mineral and provide unit dimension of structure (Celik *et al.*, 2008). Diffractograph demonstrated a predominant phase of quartz and dolomite. This pattern of fraction clears the disappearance of dolomite and clay fraction comprises by phyllosilicates.

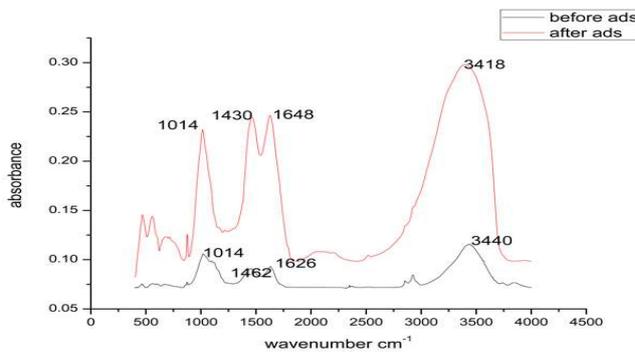


Fig. 2: Infra-red spectrum of Fabric Fly Ash before and after adsorption

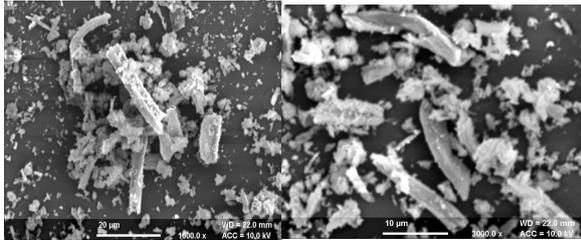


Fig. 3 Morphological structure of Fabric Fly Ash

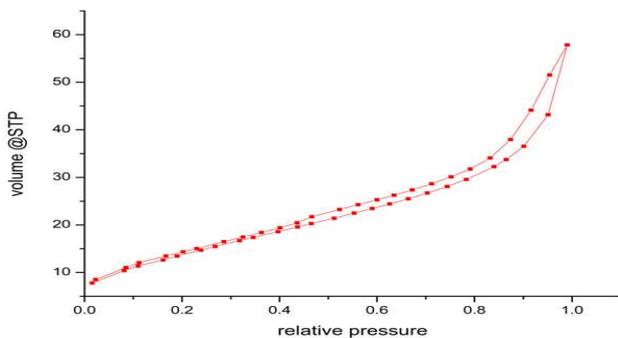


Fig. 4: BET Nitrogen adsorption-desorption isotherm of Fabric Fly Ash

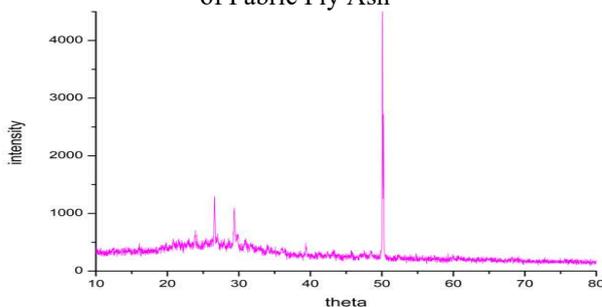


Fig. 5: XRD image of Fabric Fly Ash

Effect of pH

pH is a controlling factor in the adsorption process, and it also affects the toxicity of metal ions. The % removal of Cadmium by fabric fly ash increased as pH of the solution increased, and the maximum % removal (90%) is obtained at pH 6.8, on this value, it attains an equilibrium after this no further

variation obtained, whereas % removal of Nickel ion decreased for high pH value as for low pH value % removal increased up to 65% because of the reason that at low pH protons released, therefore competition of metal ion with protons. This behavior completely depends upon the nature and properties of adsorbent (Anagho *et al.*, 2013; Prabakaran *et al.*, 2012).

Effect of adsorbent dose

Adsorbent dose effect studied on varying quantity from 0.1 to 0.3g in 15ml of 25ppm stock solution and rotary shaker was employed for shaking purpose for constant 2h. This optimization factor decides the optimum range of adsorbent used in the further experiment. The results showed that for Cadmium ion as well as for Nickel ion, optimum range is 0.1 g for the adsorbent. The effect of adsorbent dose onto the adsorbate ions revealed that on varying adsorbent dose % removal increased. For 0.2 g and 0.3 g adsorption capacity increased which means that as increased of the amount of adsorbent percentage removal and adsorption increased due to the availability of the more active sites. The similar observations are reported (Essomba *et al.*, 2014).

Adsorption isotherms

To know the mechanism of adsorption, isotherms can be used to predict the accumulation of substance. Langmuir, Temkin isotherms were used to predict adsorption potential. Langmuir isotherm gives knowledge of monolayer adsorption. It also assumes that adsorption takes place at the homogenous surface. Langmuir equation is (Kumar *et al.*, 2009)

$$q_e = K q_0 C_e / 1 + K C_e \quad \dots (1)$$

q_0 is maximum monolayer capacity (mg g^{-1}), and K is Langmuir constant (L mg^{-1}). The plot of $1/q_e$ vs. $1/C_e$ gives slope and intercepts value for calculation of monolayer capacity. But this isotherm doesn't give straight line and also negative intercept value, same kind of work reported by (Kiurski *et al.*, 2012). Temkin isotherm is one that shows adsorbate-adsorbent interactions and also explains the logarithm coverage layer information. Equation presented by Temkin (Srivastava *et al.*, 2011)

$$q_e = B \ln A_t + B \ln C_e \quad \dots (2)$$

where $B = \frac{RT}{b_t}$ constant related to the heat of adsorption (J mol^{-1}) A_t equilibrium binding constant (l g^{-1}) and b_t Temkin isotherm constant. The plot between q_e and $\ln C_e$ gives straight line presented in Fig. 6 and slope or intercept values helps to calculate all parameters to define this adsorption isotherm.

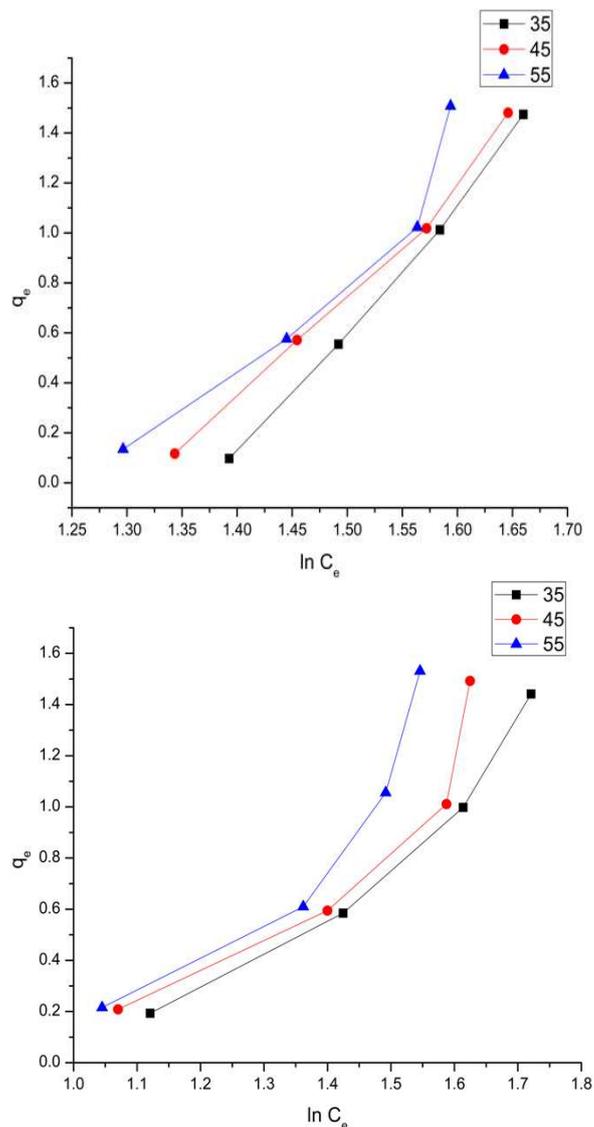


Fig. 6: Temkin isotherm at different Temperatures (a) Cadmium (b) Nickel

Temkin isotherm was studied concerning three temperatures 35 °C 45 °C and 55 °C. From the plot, it is proved that as the temperature increasing adsorption capacity per gram of adsorbent increasing from 35 °C to 55 °C. Parameters calculated such as Temkin binding constant increased from 0.722 to 0.903 for Cadmium ion as temperature increased. On the other hand, the heat of adsorption decreased from 5.115 to 4.189 as temperature increased. Similar kind of behavior is shown by Nickel metal ion (Rao *et al.*, 2014). All the calculated parameters are shown in Table 2.

Chemical Kinetics

Kinetics behaviour shows the efficiency of the adsorbent and speed of adsorption, adsorption constant and desorption constant values for fabric fly ash adsorbent. Kinetics also decides the order of reaction and how adsorption capacity takes place concerning time variations.

Langrange pseudo second order behavior is given by equation

$$t/q_t = 1/(K_2q_e^2) + t/q_e \quad \dots (3)$$

where K_2 second order rate constant ($\text{g mg}^{-1} \text{min}^{-1}$). Adsorbent for Cadmium and Nickel metal ions adsorption comes under second-order behavior concerning linear correlation R^2 . The plot between t/q_t and t (Fig. 7) gives quiet well fit in the form of a linear line and slope and intercept values for calculating other factors. This study performs for three temperatures of 35 °C, 45°C and 55 °C, as temperature increased the amount adsorbed per gram of adsorbent decreased for both metal ions, similar trend reported by (Muthuselvi *et al.*, 2016; Venkatesan *et al.*, 2016; Panayotova *et al.*, 2001; Patil *et al.*, 2012).). Weber-Morris model is also known as the Intra-particle diffusion model which determines the rate of adsorption of any liquid system.

$$q_t = K_i * t^{0.5} \quad \dots (4)$$

Where K_i intra diffusion rate constant ($\text{mg g}^{-1} \text{min}^{-1/2}$)

This equation shows time expansion of concentration (Tsibranska *et al.*, 2011).

Fig. 8 explains initial concentration behaviour of diffusion rate and as demonstrated by

figure linear curve that does not pass through origin which means that diffusion takes place by the help of other models also. No boundary layer effect noticing here and it is not rate limiting or controlling step. Figure between q_t vs. $t^{0.5}$ explain the linearity of the equation with respect to high value of correlation coefficient for both metal ions and all factors calculated as shown in Table 3.

Elovich kinetic equation is given by

$$q_t = 1/\beta [\ln(\alpha\beta)] + \ln t/\beta \quad \dots (5)$$

where α and β are adsorption and desorption constant. This model also describes the second order kinetic behavior as demonstrated by fig. 9 and same trend reported by (Tan *et al.*, 2009) Desorption constant going to increase upon increased temperature for both the metal ions which is an indication of extent surface area coverage for the adsorbate molecules to adsorb.

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Conclusion

Adsorption on Fabric Fly Ash is found as a effective strategy. Fabric Fly Ash demonstrated as an effective and ease adsorbent. Adsorption subject to pH and adsorbent measurement, to optimize pH 6.8 and adsorbent dosage estimation of 0.1 g. Adsorption mechanism is very much clarified by Temkin isotherm and all parameters assessed from this isotherm gives linearity with temperature esteems. Dynamic models clarify the efficiency of the adsorbent. Kinetic

behaviour takes after the pseudo-second-order show. All models Pseudo-second order, Intra particle dispersion, Elovich condition and Natrajan and Khalaf arrange give well fit concerning the direct relationship coefficient.

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